



**WASSER
3.0**

FACTSHEET

WASSER 3.0 PE-X®

Simultaneous Microplastic & TSS Removal at
a Municipal WWTP – Mykonos, Greece

86%

MP Removal (mass)

95%

TSS Removal

70%

COD Reduction

93%

Turbidity Reduction



REMEDIES
MEDITERRANEAN SEA BASIN LIGHTHOUSE

 Co-funded by
the European Union

OVERVIEW

This factsheet summarizes the results of pilot trials conducted at the municipal wastewater treatment plant (WWTP) of Mykonos, Greece, within the EU Horizon Europe REMEDIES project (GA 101093964). The Wasser 3.0 PE-X® pilot unit was installed downstream of the two-stage conventional activated sludge (CAS) line and operated in semi-continuous mode over five experimental loops.

DEMO SITE – MYKONOS WWTP

Location	Mykonos Island, Cyclades, Greece
Design capacity	48,000 population equivalents (PE)
Off-season population	< 10,000 PE
Treatment lines	Conventional activated sludge (8,400 m ³ /d) + MBR (10,800 m ³ /d; shut down during trials)
Wastewater sources	Municipal sewage (sewer network) + septic tank deliveries by truck
Discharge	Mediterranean Sea (Aegean)

TECHNOLOGY

Process	Wasser 3.0 PE-X® Agglomeration-Fixation Technology (Clump & Skim)
Reactor capacity	200 L (reactor) + 800 L (separation unit), stainless steel
Flow rate	5 m ³ /h (semi-continuous mode)
MP reagent	abcr eco Wasser 3.0 PE-X®, wastewater (AB930003), 5 mL per loop
MP detection	Fluorescence staining (Wasser 3.0 detect mix MP-1) + Zeiss Axiozoom.V16 microscopy, 10 µm detection limit
TRL	8+ (municipal WWTP application)
TRL	9 (industrial wastewater treatment)

KEY RESULTS

MP influent	633–5,843 MP/L (mean 2,032 ± 2,176 MP/L)
MP effluent	96–263 MP/L (mean 178 ± 76 MP/L)
MP removal	86 ± 8% (range 77–96%)
TSS influent	43–515 mg/L (mean 194 ± 173 mg/L)
TSS effluent	2–14 mg/L (mean 7 ± 5 mg/L)
TSS removal	95 ± 3% (range 91–99%)
COD influent	95–786 mg/L (mean 323 ± 254 mg/L)
COD effluent	51–56 mg/L (mean 53 ± 2 mg/L)
COD removal	70 ± 20% (range 46–93%)
Turbidity removal	93 ± 7% (82–99%), effluent 2–3 NTU
pH / Conductivity	Stable; pH 6.9 → 7.2, conductivity unchanged (15.6 mS/cm)
MP size distribution	70% of influent MP < 50 µm; larger particles removed more efficiently

REGULATORY COMPLIANCE

After treatment, all effluent values comply with Greek/EU discharge limits (COD ≤ 125 mg/L, TSS ≤ 35 mg/L) as required by JMD oik. 5673/400/1997 transposing Directive 91/271/EEC. Untreated WWTP effluent exceeded these limits in multiple loops. The revised EU Directive (EU) 2024/3019 mandates MP monitoring from 2025 (Article 17), with transposition by July 2027. All reagents are EU-REACH compliant.

KEY ADVANTAGES

Filter-free	No fouling, no clogging – agglomerates > 1 mm separated via coarse-pored units
Robust	Stable performance despite irregular truck-delivered wastewater with high variability
Circular economy	Agglomerates are recyclable (construction materials, energy recovery)
Cost-effective	-20% lower CapEx, up to 75% lower OpEx vs. membrane filtration
Dual removal	Simultaneous MP + TSS removal in a single process step
Scalable	Modular containerised systems (250 L-1,000 L) for rental & service model

FUNDING & REFERENCE

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Publication	<p>Sturm, M.T.; Argyropoulou, D.; Ronsse, P.; Korzin, A.; Schober, D.; Myers, E.; Eleftheriou, A.G.; Lelekis, I.; Galani, A.; Schuhen, K. Simultaneous Removal of Microplastics and Total Suspended Solids from Wastewater via a Novel Organosilane-Induced Agglomeration-Fixation Method at a Two-Stage Treatment Plant in Greece. <i>Clean Technol.</i> 2026, 8, 32.</p> <p>https://doi.org/10.3390/cleantechnol8020032</p>
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